

# Carbon-Free Fuels in Gas Turbines, for Propulsion & Power



FT4000® Aeroderivative Dual Fuel Gas Turbine Engine.

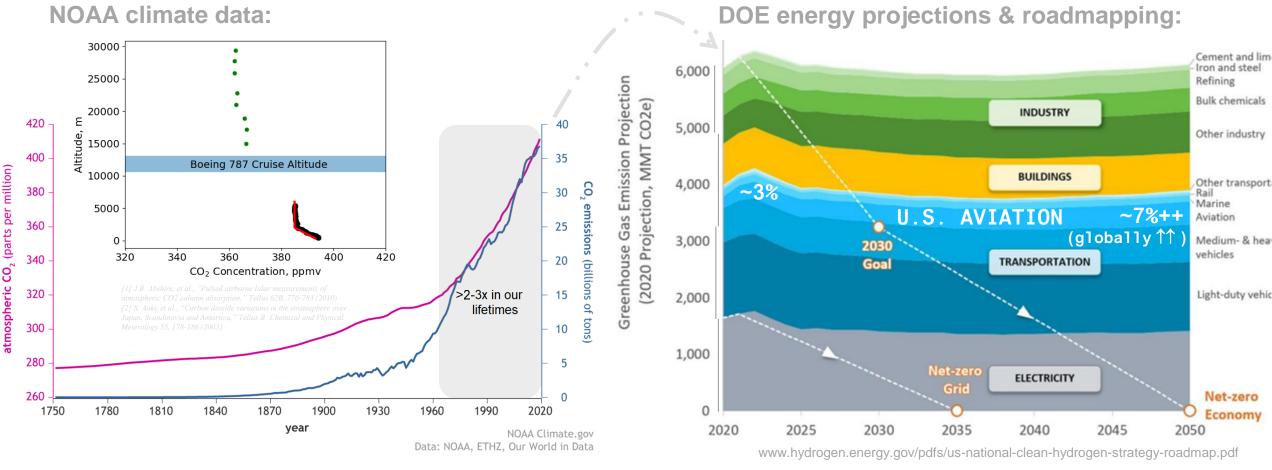




Carbon-Free Fuel Combustion Workshop
Boston, MA, 16 March 2025
14<sup>th</sup> US National Combustion Meeting (USNCM)



## **Context**: Gas Turbines' Contribution to CO<sub>2</sub> Emissions



- Aviation contributes ~3%+++ of anthropogenic CO<sub>2</sub> emissions ..... in US & Globally ......
- Aviation is challenging to de-carbonize → long service life & "energy dense" power needed
- Power generation Gas Turbines contribute + ~10% CO<sub>2</sub> emissions in US

Gas Turbine

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> Shipping CO<sub>2</sub> emissions similar level as Aviation globally: fewer GTs but more fuel-flexible

## Hydrogen-based Engines (incl. NH<sub>3</sub>) ... re-visit for new (& old) reasons

#### Early Cold-War Era:

high-altitude, high-speed flight



NASA X-15

➤ NH<sub>3</sub> fueled

rocket engine

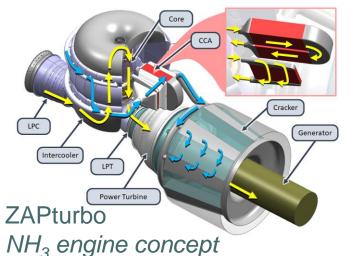


Project Suntan
 ➤ H<sub>2</sub> turbine engine,
 predecessor to RL10

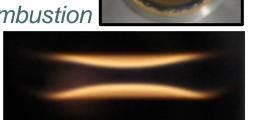
rocket engine

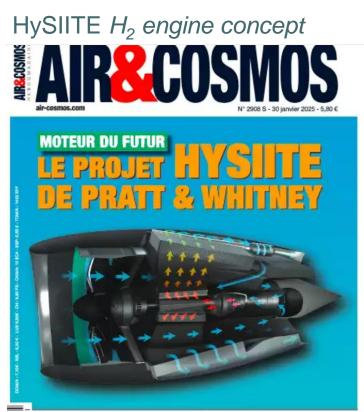
#### Climate-Change Era:

low carbon, low climate-impact flight







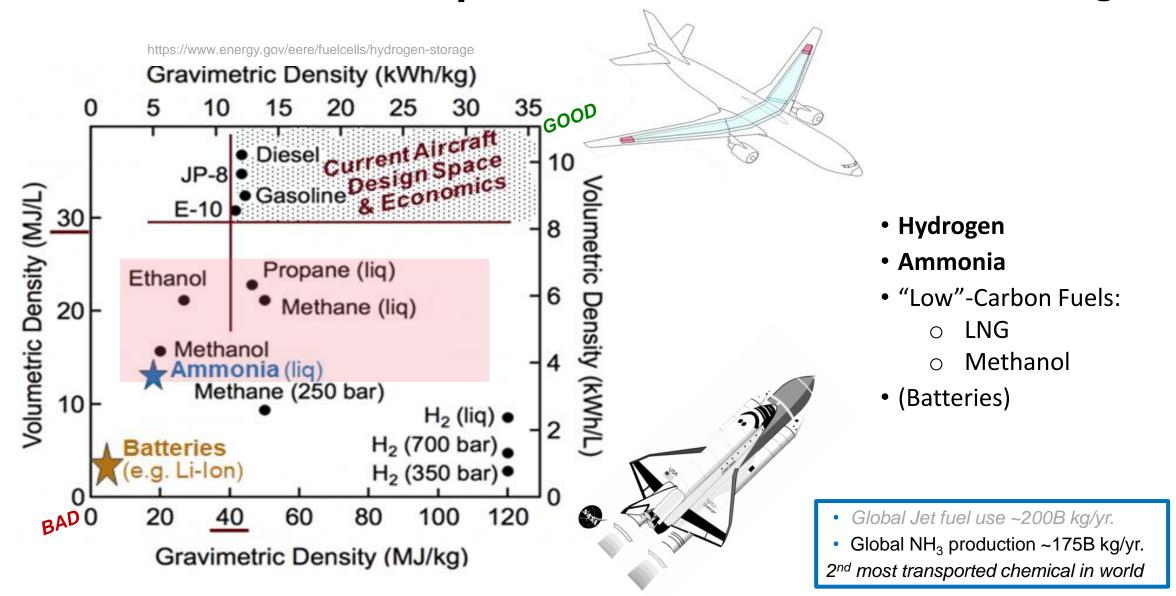








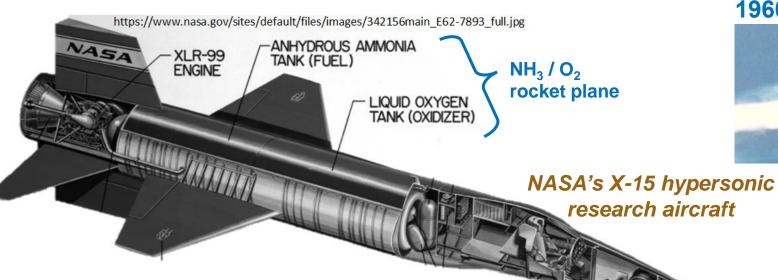
## "Net-Zero Carbon" Fuel Options in Aviation: Volume & Weight





Ammonia's energy similar to Methanol; Storage properties similar to Propane → "familiar" fuel

## NH<sub>3</sub> as a useful propulsion fuel: How (or Why)



1960 ... 1<sup>st</sup> flight of NH<sub>3</sub>-powered aircraft







XLR-99 rocket engine: propellant =  $NH_3 / LOx$ 

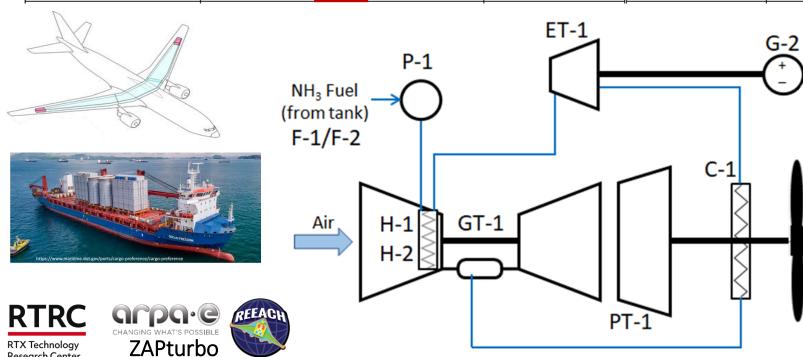
<u>WHY</u>?

- NH<sub>3</sub> chemically stable
- NH<sub>3</sub> easily liquefied (-33C)
- NH<sub>3</sub> has excellent properties for nozzle cooling -- better cooling & thrust than ethanol/water, & pre-dates RP-1 & LH<sub>2</sub> developments
- NH<sub>3</sub> does not coke  $\rightarrow$  **Able to absorb significant heat**

And has zero carbon!

## Beyond Storage: Fuel Properties for Cooling & Working Fluid

Performance Metrics, for <u>Low-Carbon Fuel Options</u>		Units  w/LHV fuel energy (Lower Heat. Val.)	<b>LH2</b> Liquid Hydrogen	NH3 Anhydrous Ammonia	Liquid CH4 / "eLNG"  e.g. SpaceX,  Blue Origin	SAF or Jet-A (state of art)
Thermal & Thermodynamic Properties	Thermal Conductivity, k	W/m-K (liquid)	0.1	0.6	0.2	0.1
	Heat Capacity, Cp	kJ / kg-K (liquid)	9.7	4.5	3.5	2.0
	"Gamma" ratio, Cp/Cv	in gas state	1.4	1.3	1.3	< 1.05 (C8+)
	Heat of Vaporization, h_fg	kJ / kg	446	1370	510	350
	Heat of Cracking reaction	kJ / kg	N/A	2700	N/A	coking issues



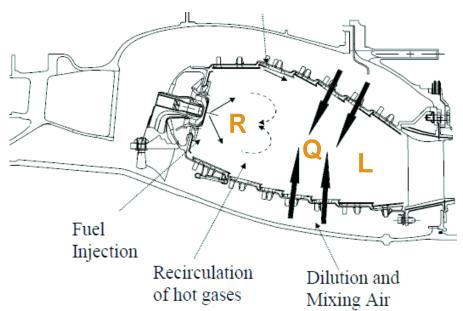
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- Thermal energy captured in fuel goes to <u>top</u> of Brayton cycle when burned
  - high-efficiency heat re-capture! (recuperation effect)
- NH<sub>3</sub> <u>liquid</u> esp. useful as working fluid, for i-cooling & in bottom. cycle
  - > cycle opportunity for GTs using large cold-liquid storage:
    - aeroderivative power incl. ships
    - also note LNG opp.

## Challenge: How to Burn NH<sub>3</sub> with low NOx emissions?

#### Re-think approach to RQL combustion...

"Conventional" RQL, e.g. hydrocarbon fuels (NG, Jet...):



- Rich-zone considerations:
  - PM (soot) vs. turndown → FAR range
  - Ignition/stability  $\rightarrow$  geom./size ( $\tau_{AnchorZone}$ )
- Lean-zone considerations:
  - CO burnout vs. NOx  $\rightarrow \tau_{\text{Lean}} \uparrow \text{or} \downarrow$ , rapid mixing
  - PF (temp. uniform.) → complete mixing

-CRN-phi=1.3\_P 70  $NH_3$ -Air Combustion at p = 35 atm, T = 850 K -CFD-phi=1.3 300 150 (mdd) **Equilibrium** 250 125 NH<sub>3</sub> @ 40 ms 2 200 150 Equilibrium 100 50 — CRN-phi1.25\_PSR1\_1.6ms CFD - swirler phi=1.25 ---- CFD - swirler phi=1.30 1.0 Equivalence Ratio  $\phi$  New/Different considerations for NH<sub>3</sub>: ■ Drive N-species to  $N_2 \rightarrow \tau_{Rich} \uparrow \uparrow$ ■ FAR<sub>RICH</sub> determined by chem. equilib. ■  $NOx_{THERMAL}$  = rapid mixing *w/less Q*<sub>AIR</sub>

Rich-Quench-Lean (RQL) reconfigured for low-NOx NH<sub>3</sub> combustion:



## DOE / NETL-sponsored project on NH<sub>3</sub> combustion studies

Low-NOx Operable Ammonia-Combustor Development (LOAD-Z)

#### RTRC UConn

year-4

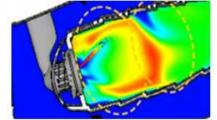
year-3

year-2

year-1

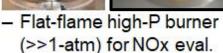
Time

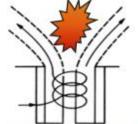




- Single-nozzle high-pressure combustor, fired w/NH<sub>3</sub> fuel
- Measure emiss. & performance: NOx, efficiency, stability





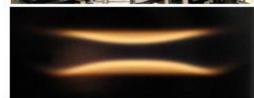


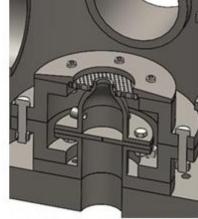
- 1-atm swirl-stab. burner
- Piloting studies w/H<sub>2</sub>

#### Modeling:

- CFD for design
- Kinetic improve.
   w/ exp. data
- CFD & validation
- Turb. models for NH3 comb. & NOx (no post-process.)
- CRN modeling
- Counterflow
- Kinetic mech.







Turbulent S<sub>L</sub> rig, for
 NH<sub>3</sub> @ P, T > ambient
 (~20% turb. intensity)

- Counterflow flame rig, compatible w/NH<sub>3</sub> fuel
- Measure strained flames w/ inlet P, T > ambient



Is it real?

(can we really get low-NOx NH<sub>3</sub>

combustion)

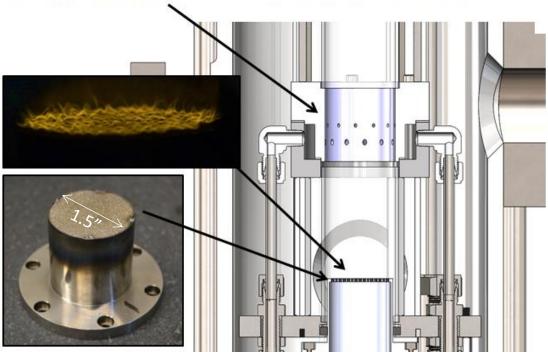
## RTRC Lab Evaluation: Pure NH<sub>3</sub> combustion @ elevated P, T

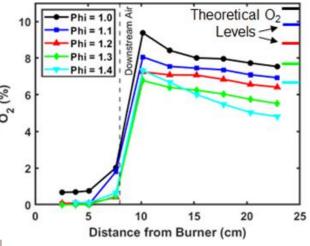
#### Preliminary data shows 35ppm NOx in 5-atm pressure RQL "burner"

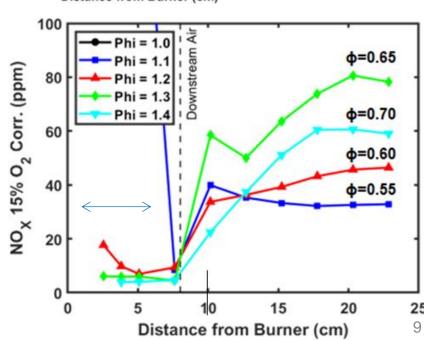


# Flat-Flame Burner Rig – Downstream Air Addition

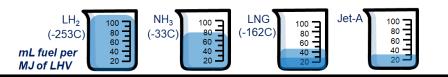
- Data collected at P = 5 atm, T<sub>in</sub> = 450 K
- Downstream air injection flowrate matched with burner air to allow for rich-to-lean transition (50 / 50 airsplit)
- Air injection ring located 8-cm downstream of burner







## What about H2...: Storage Vol. & Temp.



Performance Metrics, for <u>Low-Carbon Fuel Options</u>		Units  w/LHV fuel energy (Lower Heat. Val.)	LH2 Liquid Hydrogen	NH3 Anhydrous Ammonia	Liquid CH4 / "eLNG"  e.g. SpaceX,  Blue Origin	SAF or Jet-A (state of art)
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	"Gamma" ratio, Cp/Cv	in gas state	1.4	1.3	1.3	< 1.05 (C8+)
	Heat of Vaporization, h_fg	kJ / kg	446	1370	510	350
	Heat of Cracking reaction	kJ / kg	N/A	2700	N/A	coking issues
Fuel Storage Requirements	Specific Energy	MJ / kg	120	18.6	50	43
	Energy Density of liquefied fuel	MJ / L	8.5	12.7	21.1	34
	Tank conditions	°C (K) atm	−253 °C (20 K) 1 atm	−33 °C (240 K) 1 atm	–162 °C (111 K) 1 atm	ambient

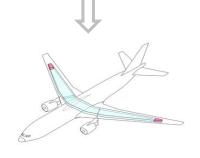


**RTRC** 

RTX Technology Research Center

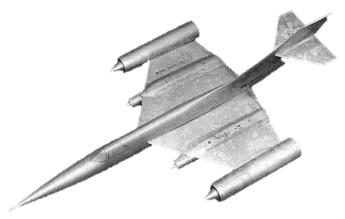


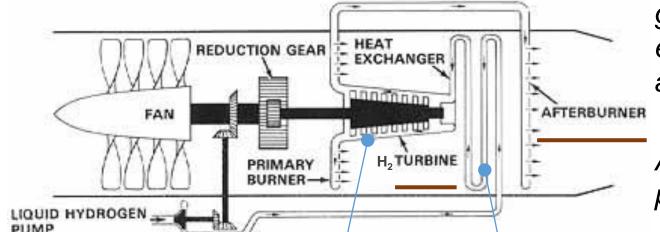




### H₂ ENGINE EXPERIENCE / LESSONS: P&W 304 ENGINE → USE THE COLD

- 1950'S PROJECT SUNTAN . . . MACH-2.5 AFTERBURNING ENGINE
- LEARNING PAVES WAY FOR P&W DEVELOPMENT OF RL10 ROCKET ENGINE

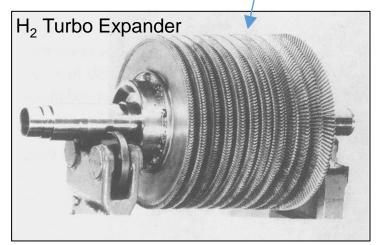


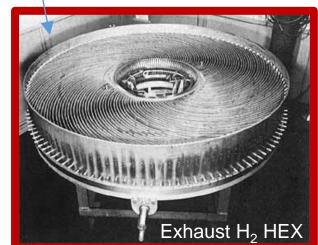


Power is generated by expanding LH2 after HEX

Augmentor provides thrust







## Hydrogen-Enabled performance → Water as Working Fluid

#### • For *aircraft* propulsion:

- condense water from high-moisture exhaust (H<sub>2</sub> combustion)
- > inject water/steam into cycle
  - high-efficiency "combined-cycle"
  - low-NOx, stable H<sub>2</sub> combustion

#### • For *power-generation*:

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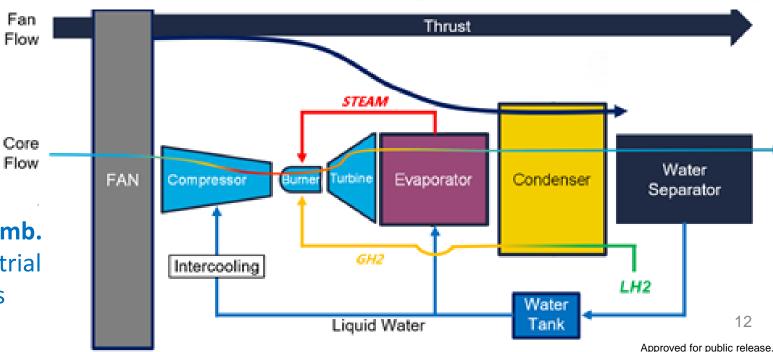
- condense or use other water source
- > inject steam into combustor & turbine
  - low-NOx H<sub>2</sub> combustion (high dilution)
  - and cycle efficiency benefit
     (e.g. H<sub>2</sub>-fired Cheng cycle)
- Applicable to aero-derivative engines & comb.
   incl. transportation (shipping), and to industrial
   or frame GTs

Hydrogen Steam Injected Intercooled Turbine Engine



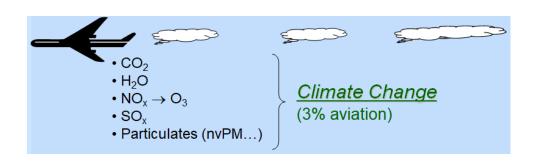
Hydrogen combustion in steam-air mix —

Stable combustion to 0.8 steam-air ratio Measured 99.3%  $NO_x$  reduction



## Emissions in Aviation – Water (vapor), nvPM, NOx & SOx

Performance Metrics, for <u>Low-Carbon Fuel Options</u>		Units w/LHV fuel energy (Lower Heat. Val.)	<b>LH2</b> Liquid Hydrogen	NH3 Anhydrous Ammonia	Liquid CH4 / "eLNG"  e.g. SpaceX,  Blue Origin	SAF or Jet-A (state of art)
Environmental	CO <sub>2</sub> emissions from engine	kg / GJ	ZERO	ZERO	<b>55</b> ( ↓ 24% vs. Jet-A )	72
	H <sub>2</sub> O emissions	kg / GJ	75	85	45	30
Impact	NOx	g / kg_fuel	target same as SAF	target same as SAF	< SAF	(1-)10-30
(emissions)	SOx	g/kg_fuel	ZERO	ZERO	ZERO	~ 1.0
	nvPM	g/kg_fuel	ZERO	ZERO	<< SAF	~ 0.1





Contrails: Studies underway

Carbon-Free fuels produce no nvPM

(nucleation sites)

But they emit more water – impact uncertain...



## Gas Turbines in Prop. & Power → Carbon-Free Fuel Opportunities







#### 3 Key Take-Aways:

- > Aviation difficult to de-carbonize, but new fuels offer efficiency improvements to help enable
- NH<sub>3</sub>: Ammonia viable as a <u>high-efficiency</u> transportation fuel incl. in aviation
  - technology spinoffs to power-gen, esp. when NH<sub>3</sub> stored as refrig. liquid (for use as working fluid)
- > H<sub>2</sub>: Hydrogen has challenges, but brings opportunity as <u>cryo</u>-fuel / cryo-fluid in aviation



## **BACKUP**



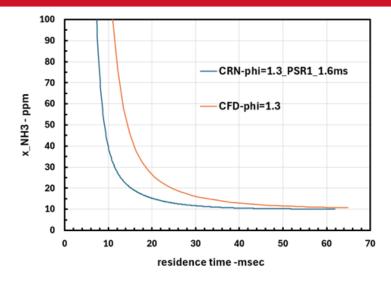


Figure 5.3 x\_NH3 vs residence time, T3=850F, T\_fuel=310.9K, Swirler φ=1.3

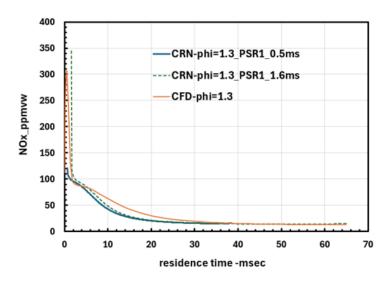


Figure 5.4 NOx vs residence time, T3=850F, T\_fuel=310.9K, Swirler φ=1.3



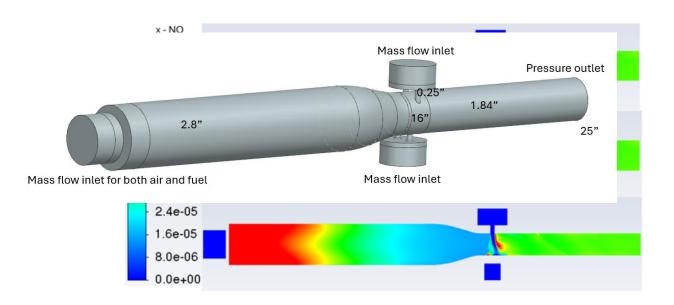


Figure 5.8 x<sub>a</sub>No, T3=850F, T<sub>a</sub>fuel=310.9K, Swirler φ=1.3

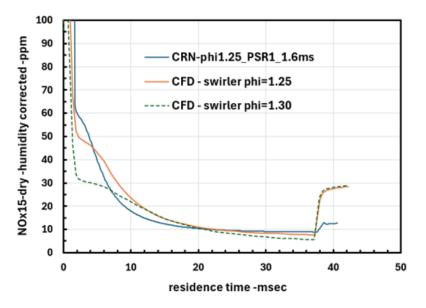
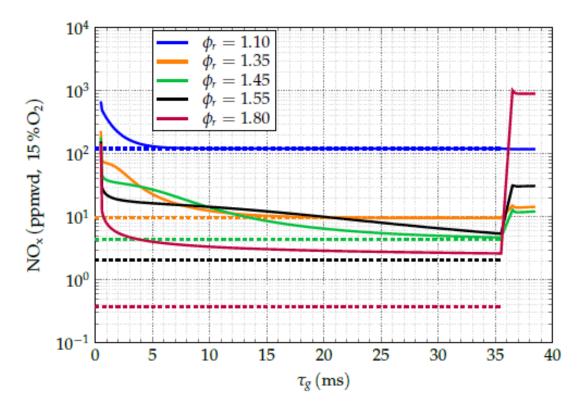
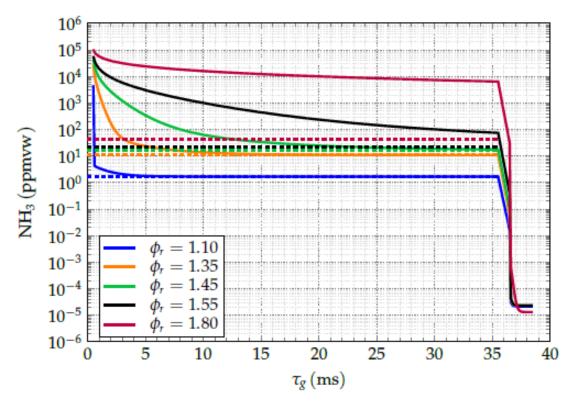


Figure 5.9 NOx15\_dry\_humidity corrected vs residence time, T3=850F, T\_sfuel=310.9K, Swirler φ=1.3

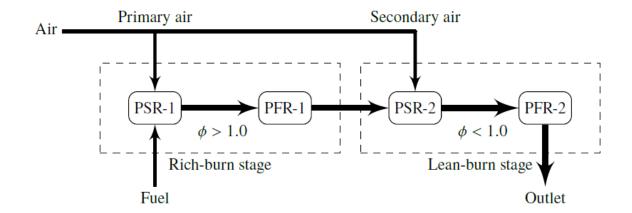
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#### (a) Evolution of NOx with global residence time

(b) Evolution of NH<sub>3</sub> with global residence time





## Re-visit NH<sub>3</sub> for <u>turbine</u> propulsion ...Physical properties...

Fuel Property	Jet-A (ambient liquid)	H <sub>2</sub> (—253 °C liquid)	NH <sub>3</sub> - anhydrous (–33 °C liquid)	
Specific Energy (MJ/kg)	43 MJ/kg	120 MJ/kg	18.6 MJ/kg	
Energy Density (MJ/L)	34 MJ/L	8.5 MJ/L	12.7 MJ/L	
T_saturation @ 1-atm (°C)	175 - 250 °C	<b>−253</b> °C	− <b>33</b> °C	
T_saturation @ 10-atm (°C)	325 - 350 °C	−242 °C	+25 °C	
Conductivity, k (W/m-K)	0.1 W/m-K	0.1 W/m-K	0.6 W/m-K	
Heat Capacity, Cp (kJ/kg-K)	2.0 kJ/kg-K	9.7 kJ/kg-K	4.5 kJ/kg-K	
Heat of Vaporization,h_fg (kJ/kg)	350 kJ/kg	446 kJ/kg	1370 kJ/kg	
Heat of Cracking reaction (kJ/kg)	coking issues	N/A	2700 kJ/kg	
"Gamma" ratio, Cp/Cv (in gas state)	< 1.05 (C8+)	1.4	1.3	

Ammonia properties are "familiar" & useful

Energy density ~ Methanol (~1/2 of Jet fuel)

Storage conditions ~ Propane

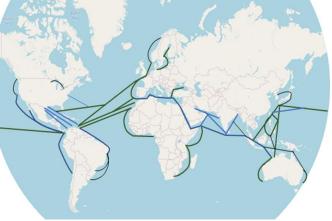
Ammonia is a well-known refrigerant, with excellent k, Cp, h\_fg

<u>Unique</u> capabilities as a fuel, with potential for <u>efficiency gains</u>



- Global Jet fuel use ~200B kg/yr.
- Global NH<sub>3</sub> production ~175B kg/yr.
- Global NH<sub>3</sub> infrastructure @ scale
   2<sup>nd</sup> most transported chemical in world

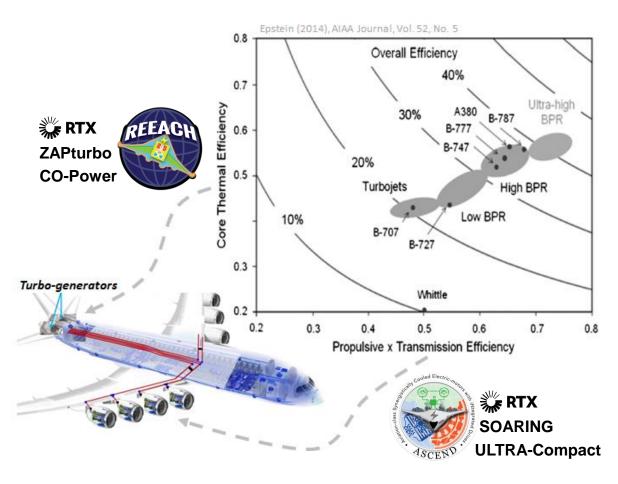






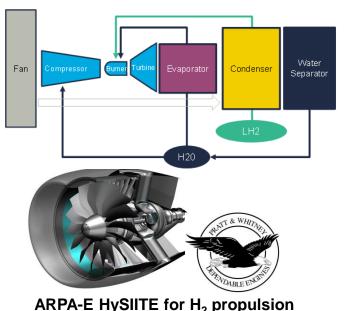
## Sustainable Aviation Technology Development ...

#### Propulsive Efficiency ↑ w/ Electrification

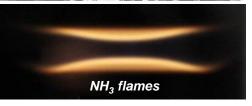


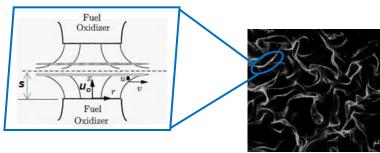
#### • Further reduce fuel weight & volume

#### Alternative Fuels for Reduced Carbon







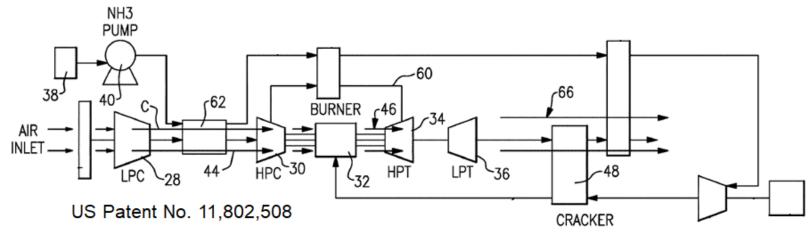


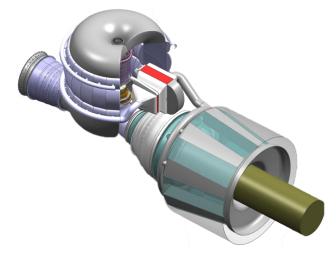
DOE-NETL "LOAD-Z" project to develop & test
 NH<sub>3</sub> combustion technology for gas turbines



# NH<sub>3</sub> Propulsion: Learned from System Studies ("where we landed")

- "Chemical recuperation" maximized by cracking downstream of NH<sub>3</sub> turboexpander
  - T<sub>HEAT SOURCE</sub> from efficient GT-cycles insufficient for high %-cracking @ high-P<sub>NH3</sub> ... (+ catalyst sintering @ high-T)
  - Maximize CC-efficiency with Q<sub>CRACKING</sub>↑ (%-cracking ↑) despite W<sub>TURBOEXPANDER</sub>↓
- NH<sub>3</sub> effective for chilling cooling-air to turbine
  - Significant cooling obtained w/ compact low-∆P HEX
  - Enables high-TRIT (T4) for efficiency & high T<sub>EXHAUST</sub> to drive cracking (90% NH<sub>3</sub> → H<sub>2</sub>)
- NH<sub>3</sub> intercooling enables high-OPR cycle
- Provides intercooling without heat rejection (without energy loss) for efficiency 1
  - NH<sub>3</sub>! NH<sub>3</sub> has ample cooling capacity at engine fuel-flow rates
    - NH<sub>3</sub> is effective liquid "refrigerant" for compact intercooling HEX





20

## Challenge: High-Pressure NH<sub>3</sub> Cracking (fight equilibrium)

Cracking: 
$$NH_3 \rightarrow \frac{3}{2}H_2 + \frac{1}{2}N_2 \dots \Delta H_{\underline{ENDO}}$$
-thermic = + 2.7 MJ/kg-NH<sub>3</sub>

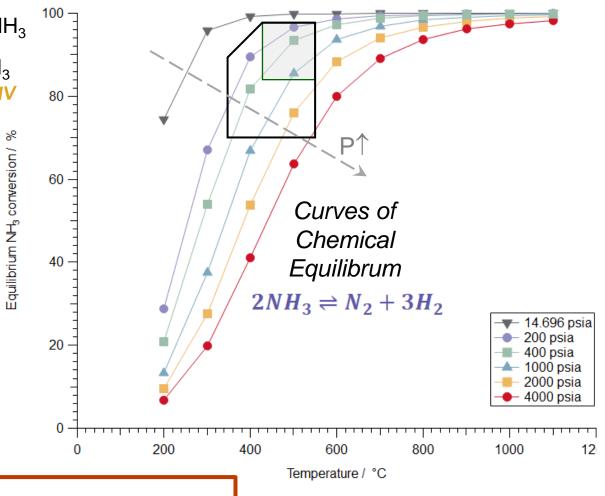
Synthesis:  $N_2 + 3H_2 \rightarrow 2NH_3 \dots \Delta H_{\underline{EXO}}$ -thermic = -2.7 MJ/kg-NH<sub>3</sub>

15% of LHV

Constraints: (design intent)

1. Avoid gas compression work (loss)

- pump liquid NH<sub>3</sub> before crack to H<sub>2</sub>
- 2. GT = internal combustion engine
  - P<sub>FUEL</sub> > **P**<sub>COMBUSTOR</sub>
- 3. Desire high %  $_{CRACKING}$  NH<sub>3</sub>  $\rightarrow$  H<sub>2</sub>
- 4. Use only waste-heat for cracking
  - T<sub>CRACKING</sub> < **T**<sub>EXHAUST</sub>

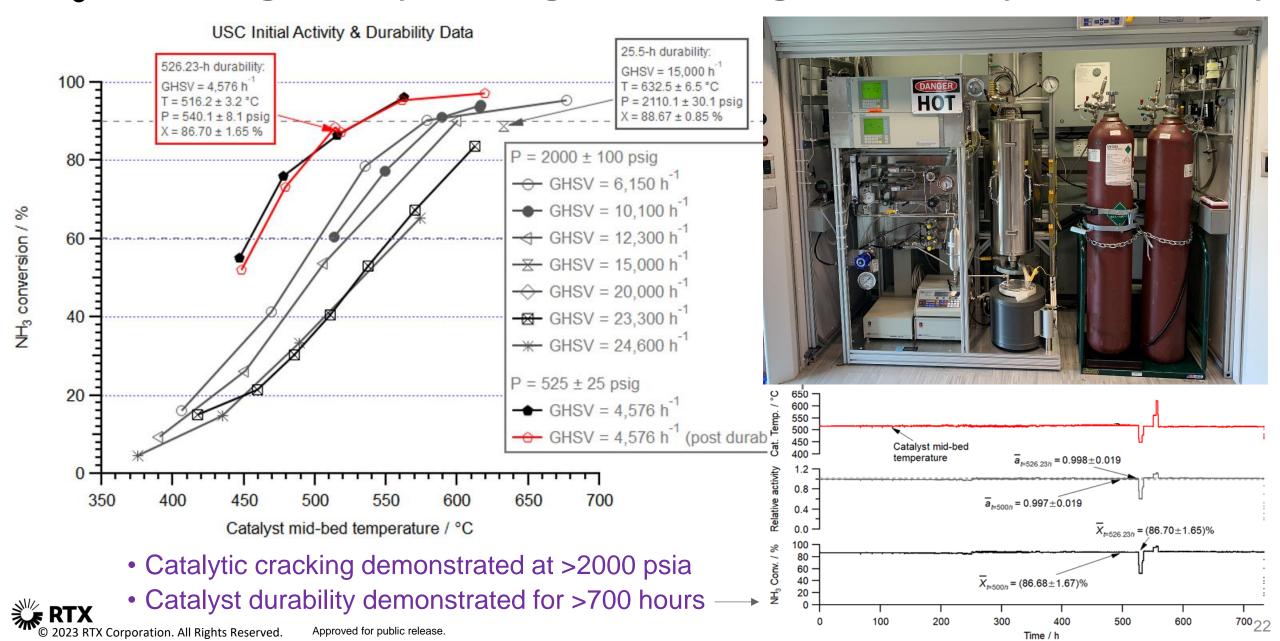


#### 2 Objectives:

- Seek optimal tradeoff: Cracking -vs.- Expansion Work
- Demonstrate catalyst activity & durability at high-P

21

## NH<sub>3</sub> Cracking Catalyst: High-P Testing for Activity & Durability



## **END**

