

# Managing risk and reliability in hydrogen systems: implications for fueling stations, forklifts, electrolyzers and beyond

**Katrina Groth** ([kgroth@umd.edu](mailto:kgroth@umd.edu))

Professor & Director, Reliability Engineering

Associate Director for Research, Center for Risk and Reliability

University of Maryland

Research supported by multiple sources. The views expressed herein are those of the authors and do not reflect the official policy or position of any sponsor.

# Fast Facts about UMD's Reliability Engineering program & Center for Risk and Reliability



**4+12**

Core, and Affiliate  
Faculty

**6**

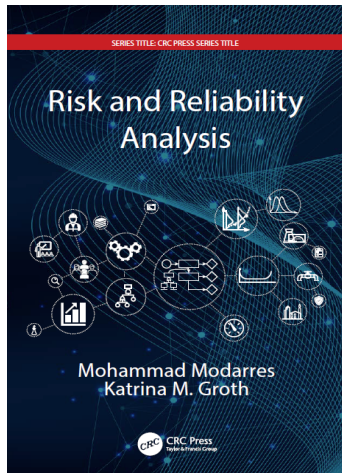
Cutting-Edge Research  
Laboratories

**4**

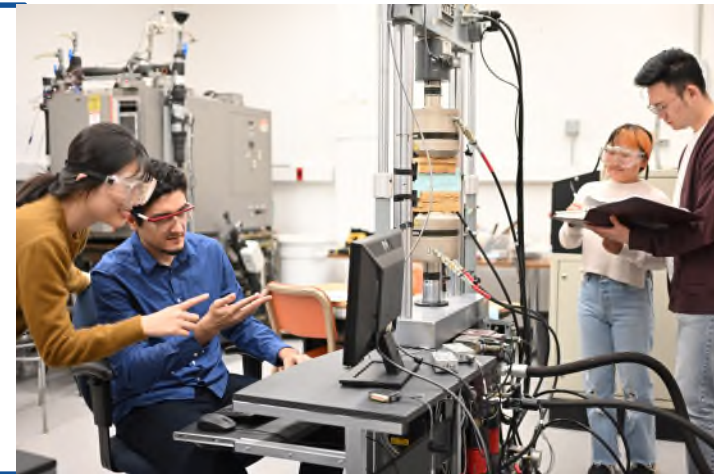
Degrees Offered  
(Ph.D. M.S., M.Eng, Certificate)

**500+**

Graduates since **1991**



- Systems Risk and Reliability Analysis Lab (SyRRA)
- Probabilistic Physics of Failure and Fracture
- Cybersecurity Quantification Lab
- Risk And Decision Analysis Lab (RADA)
- Design Decision Support Lab
- Risk-Informed Solutions in Engineering (RISE)

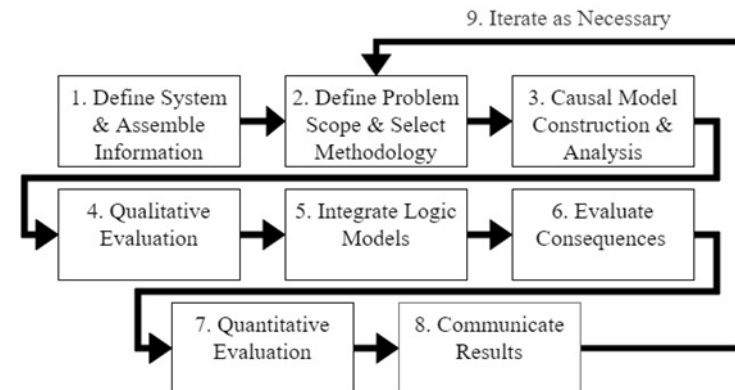
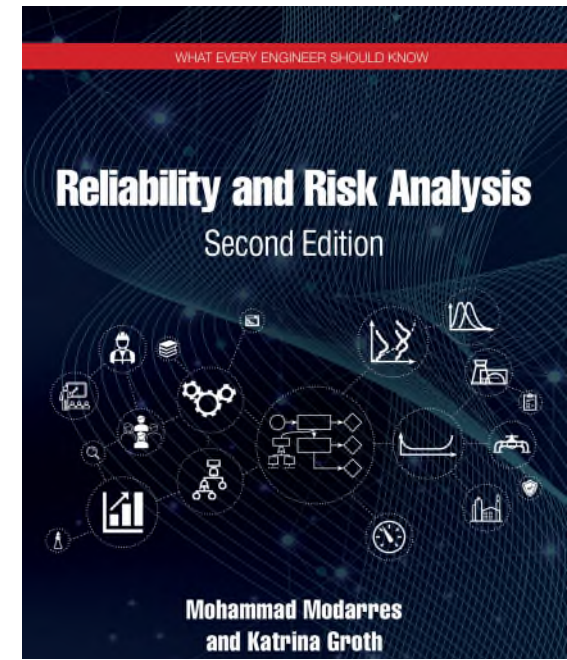


The **#1** Reliability Engineering program in the U.S. (Source: Scopus)

# Reliability engineering & quantitative risk assessment (QRA): structured processes to support decision-making



- By building understanding of:
  - **What the system is supposed to do** (performance)
  - **The sources, causes, and likelihood of failures** (physics-based, human, computational, etc.)
  - **Priorities & strategies to reduce failure** (e.g., design, operation, maintenance)
- Offers the opportunity to identify & proactively change systems & practices throughout the lifecycle



Copyright, Katrina Groth, 2025

# Application areas for reliability engineering





# Hydrogen is here – enabled by unprecedented national investment



## Bipartisan Infrastructure Law

**Includes \$9.5B for clean hydrogen:**

- **\$8B** - regional clean hydrogen hubs
- **\$1B** - electrolysis
- **\$0.5B** - manufacturing and recycling

## Inflation Reduction Act

**Includes significant tax credits**

(e.g., up to \$3/kg for clean H<sub>2</sub> production)

## U.S. Goals

Reduce 50% U.S. GHG emissions by 2030

Net zero GHG emissions no later than 2050

### Clean Hydrogen Production

- 10 MMT by 2030
- 20 MMT by 2040
- 50 MMT by 2050

### Greenhouse Gas Reduction

- 10% reduction economy-wide

### Economic Impact

- 100,000 new direct / indirect jobs by 2030

### SELECTED REGIONAL CLEAN HYDROGEN HUBS



# The hydrogen technology is global



Toronto,



Seoul, Korea (2025)



, Germany (2016)



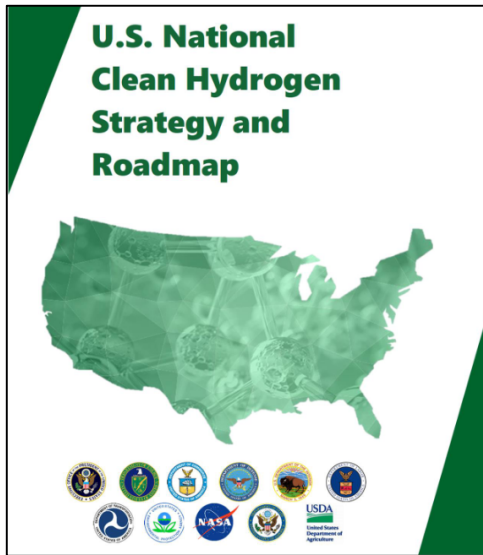
Maryland, U



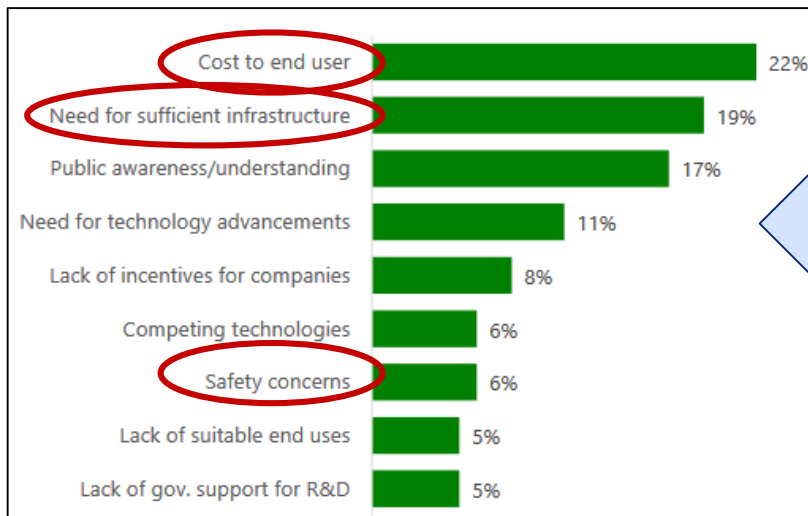
ryland, USA (2024)



# Safety & Reliability are a Key Barrier to H2 Deployments



- 2023 U.S. National Hydrogen Strategy identifies:
  - Reliability & risk assessment as key needs for enabling deployments.
  - Education: 100,000 new jobs by 2030



Survey at 2021 DOE Hydrogen Summit shows that safety and reliability dominate the key barriers to public acceptance and market adoption.

# Now we have the technology, but we do have some problems...



## Fire engulfs new hydrogen bus and fueling station at Golden Empire Transit



*Bus & Station Fire, Bakersfield, CA, Aug 2023*

*Norway fueling station explosion, June 2019  
10 stations shut down for investigation*



*Bus fire, Chungju, Korea, Dec 2024*



# And it's not just safety: the \$100M problem is **reliability**



Los Angeles Times

CLIMATE & ENVIRONMENT

## Refueling a hydrogen car in California is so annoying that drivers are suing Toyota

WIRED

BY KYLE YOUNKER BUSINESS NOV 19, 2024 8:00 AM

## The Norwegian Company Blamed for California's Hydrogen Car Woes

A civil fraud case reveals that the hydrogen fueling stations promoted by Toyota, Shell, and Chevron never worked in the first place.

USA, Nov. 2024

H<sub>2</sub> California USA, Aug. 2024

## Widespread Breakdowns Cripple Hydrogen Stations in South Korea

By FCW Team  
September 23, 2024 at 9:35 AM EDT



South Korea, September 2024

## Hyundai recalls all 1,269 of its hydrogen-powered city buses in operation in South Korea due to new safety concerns

News comes several months after an Elec City bus exploded, seriously injuring a refuelling station worker



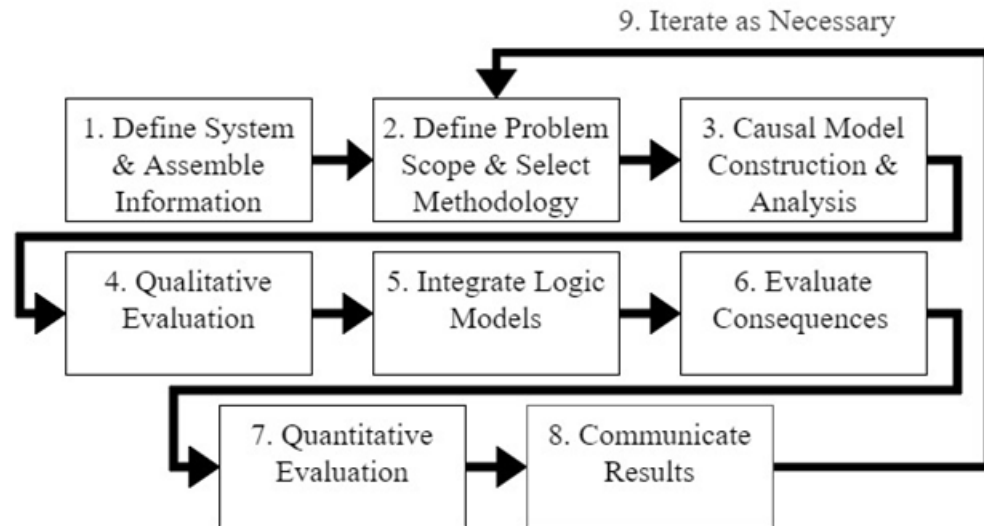
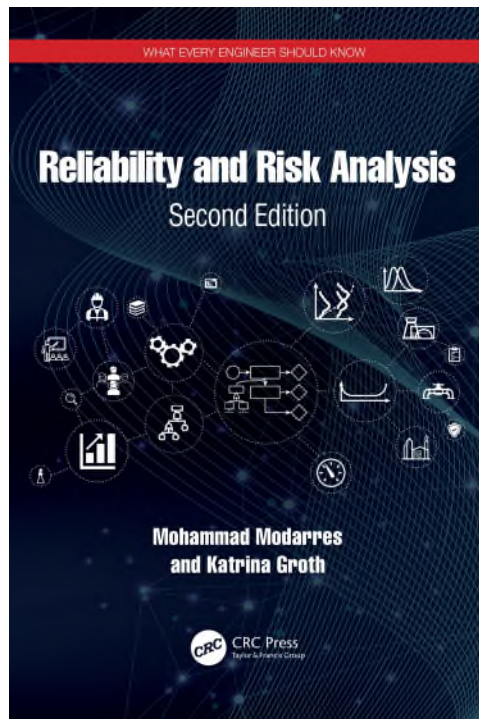
Seoul, Korea, May 2025



# Bad approaches to dealing with potential failures (risk) & safety questions



# Reliability engineering & risk analysis are part of the solution



# Selected projects: 15 years of enabling safer hydrogen equipment & pipeline deployments



**QRA for H2 indoor fueling for NFPA 2**

**QRA for H2 separation distances in NFPA 2**

**ISO 19880-1 incorporates QRA and HyRAM for safety distances & more**

**LH2 On-site storage QRA**

**Pipeline corrosion model**

**BaNTERA pipeline excavation damage model**

**H2FC Forklift QRA**

**LH2 fueling station QRA**

**PEM Electrolyzer QRAs**

**2010-2014**

**2015**

**2017**

**2019**

**2021**

**2023**

**2025**

**HyRAM algorithm**

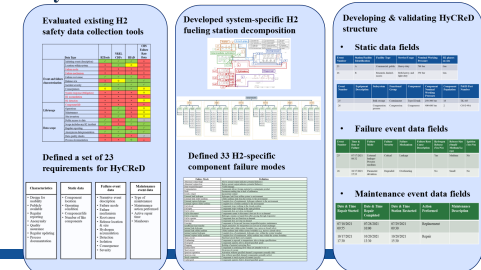
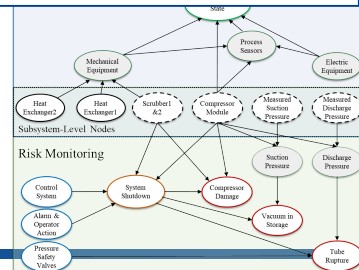
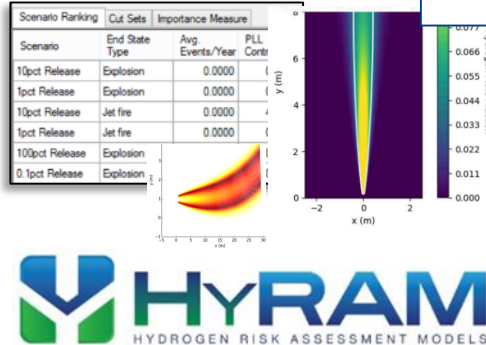
**Public release of HyRAM 1.0**

**H2 Storage Risk & Reliability Gap Study**

**PHM & QRA Data requirements for LH2 storage**

**HyCReD fueling reliability data collection framework**

**SIPPRA algorithms**





# Major research activities include:

- Risk assessment (QRA) to establish codes & standards requirements
- Reliability & risk assessment (QRA) to establish risk tolerability & dominant risk contributions & mitigations
- Prognostics & health monitoring to enable reliability prediction and intervention
- Reliability modeling & failure analysis
- Reliability data collection to set priorities

# HyRAM+: Making hydrogen safety science accessible through computational tools



Sandia  
National  
Laboratories



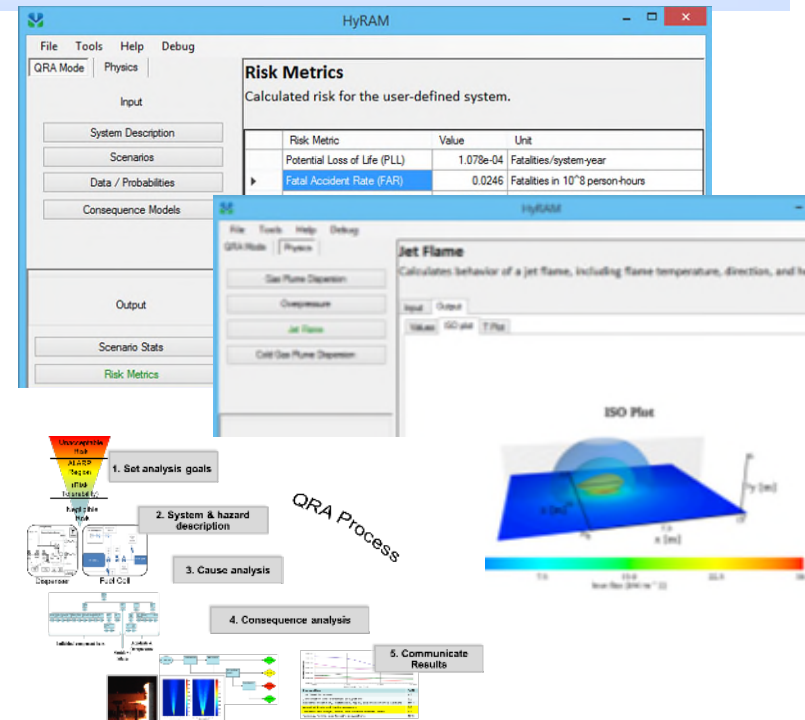
**First-of-its-kind integration platform for state-of-the-art hydrogen safety models & data - built to put the R&D into the hands of industry safety experts**

## Core functionality:

- Quantitative risk assessment (QRA) methodology
- Frequency & probability data for hydrogen component failures
- Fast-running models of hydrogen gas and flame behaviors

## Key features:

- GUI & Mathematics Middleware
- Documented approach, models, algorithms
- Flexible and expandable framework; supported by active R&D



Copyright, Katrina Groth, 2025

**Free at <http://hynam.sandia.gov>**



# Impact: QRA enabled safe deployment of hydrogen systems



- **QRA enabled the first US & International codes for H2 infrastructure**

- *NFPA2 Ch. 7*: Established GH2 separation distances (SAND2009-0874)
- *NFPA2 Ch. 10*: Calculated risk from indoor fueling (SAND2012-10150)
- *NFPA2 Ch. 5*: Enabling Performance-based compliance option (SAND2015-4500)
- *ISO 19880-1 Ch. 4*: Developed consensus approach for defining specific mitigations (e.g., safety distances) using regional criteria & requirements (2016)
- *ISO 19880-1 Annex A*: Developed safety distance & mitigation examples (2017)

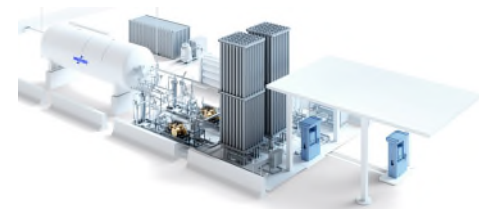


Advances in reliability engineering & safety for hydrogen systems will continue to drive the industry forward

# Quantitative Risk Assessment of hydrogen releases in a hydrogen fueling station with LH<sub>2</sub> storage



**Objective:** Perform 1<sup>st</sup> full QRA on a high-capacity hydrogen fueling station with liquid hydrogen storage (LH<sub>2</sub>), high-pressure cryogenic compression, and temperature control through GH<sub>2</sub> and LH<sub>2</sub> mixing.



## Qualitative Analysis:

Design realistic high-capacity station & FMEA



## H<sub>2</sub> Release Models:

Develop fault trees for H<sub>2</sub> release scenario



## Event Sequence Models:

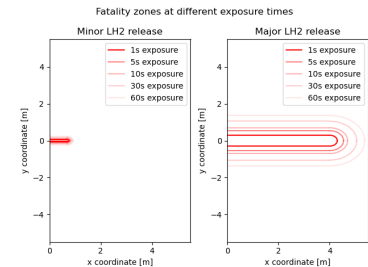
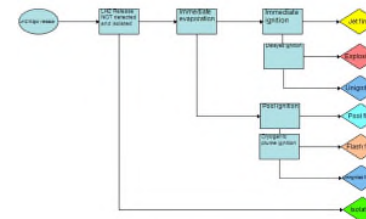
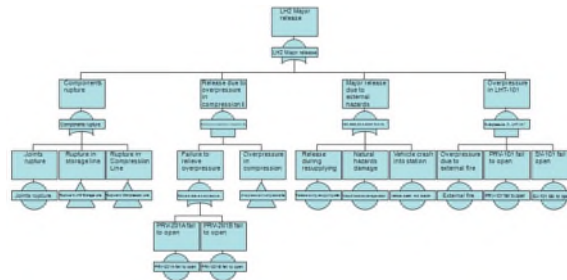
model undesired scenario progression



## Consequence Analysis:

Fatal Accident Rate & Average Individual Risk

Probability Class	High	M	H	H
	Medium	L	M	H
	Low	L	L	M
	Severity Class			
	Minor	Moderate	Critical	



## Results:

**Fully documented QRA** to act as a baseline for safety of a liquid storage high-capacity H<sub>2</sub> fueling station

### Most significant risk contributors:

- Cryogenic pump releases, H<sub>2</sub> sensor failure, Vaporizer ruptures, Filter ruptures, Valve fail. to close
- **FAR:**  $1.24 \times 10^{-1}/\text{year}$
- **AIR:**  $3.41 \times 10^{-5}/\text{year}$
- ( $< 10^{-4}$  AIR threshold of EIHP2)

## Implications & Impact:

- Provide basis for using QRA to enable reliability, siting, and standards development for liquid storage high-capacity H<sub>2</sub> fueling station
- Inform industry and stakeholders about **risks and mitigation options** for LH<sub>2</sub> station designs and technologies.
- **Demonstrated AIR within risk-tolerability zone.**

Copyright, Katrina Groth, 2025

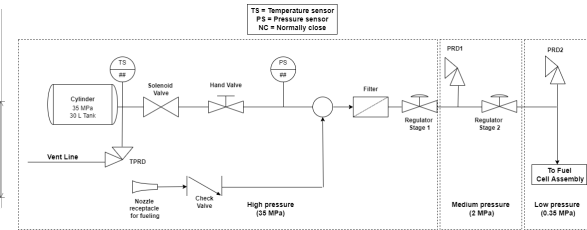
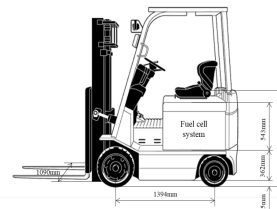




# QRA of a hydrogen fuel cell forklift



## Generic H2 forklift system design

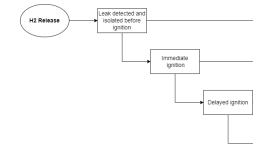


## FMEA

ID	Type	Function	Failure Mode	Cause	Local Effect	System Effect
Tank (Type III or IV)	On-board storage of gaseous hydrogen at 35 MPa	Rupture (loss of fluid and fragmentation of container beyond the 12% design pressure)	External impact damage (collider, road debris);	Explosive release of mechanical energy; stored gas and container;	Immediate ignition of released fluid	Delayed ignition of collected vapors, potential explosion or detonation hazard
			External or loaded fire damage; Inadequate design, testing, manufacturing, installation, or maintenance	Explosive release of container materials; Potential asphyxiation hazard; Collection of combustible mixture in closed environment;	Escalated gas and container release; Delayed ignition of collected vapors, potential explosion or detonation hazard	
		Leakage (loss of fluid without substantial pressure drop)	Degradation; Seal failure; External impact damage; Inadequate design, testing, manufacturing, installation, or maintenance	Potential asphyxiation hazard; Delayed ignition of collected vapors, potential explosion or detonation hazard	Immediate ignition of released fluid; Delayed ignition of collected vapors, potential explosion or detonation hazard	

Full FMEA available upon request

## Event sequences



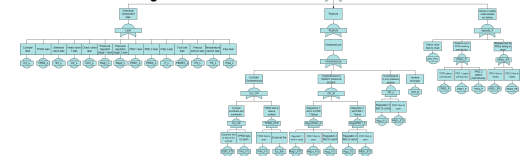
## Release & flame simulations



## Basic event frequencies

ID on Fault Tree	Description	Median (HyRAM)	Mean	Lower 5%	Upper 95%	Reference
CyLL	Cylinder leak	2.30E-07	2.83E-07	6.93E-08	7.87E-07	[29]
Vent.L	Vent line leak	8.08E-07	3.89E-09	5.48E-06		[29]
TPRD.L	TPRD leak	2.60E-03	7.40E-04	5.38E-03		[36]
SV.L	Solenoid valve leak	4.80E-06	1.24E-05	3.30E-07	7.09E-05	[29]
HV.L	Hand valve leak	4.80E-06	1.24E-05	3.30E-07	7.09E-05	[29]
CHV.L	Check valve leak	8.29E-05	3.19E-07	3.32E-04		[36]

## FT analysis



## Total risk (FAR, AIR)

		AIR.		FAR		Expected
		fatalities/forklift-year		fatalities/100 million hours-driver		fatalities/year
Release scenario	Pressure section	Jet Fire				
Minor release	Low	0	0	0		
	Medium	0	0	0		
	High	0	0	0		
Major release	Low	$3.27 \times 10^{-6}$	0.16	$6.53 \times 10^{-2}$		
	Medium	$2.74 \times 10^{-6}$	0.14	$5.48 \times 10^{-2}$		
	High	$3.49 \times 10^{-5}$	2.77	1.11		
Total		$4.09 \times 10^{-5}$	3.07	1.23		
Explosion						
Minor release	Low	0	0	0		
	Medium	0	0	0		
	High	0	0	0		
Major release	Low	$1.41 \times 10^{-6}$	0.02	$2.82 \times 10^{-2}$		
	Medium	$1.36 \times 10^{-6}$	0.07	$2.72 \times 10^{-2}$		
	High	$2.67 \times 10^{-5}$	1.34	$5.34 \times 10^{-1}$		
Total		$2.95 \times 10^{-5}$	1.42	$5.90 \times 10^{-1}$		

## Component Risk Reduction Worth

High Pressure			
Fault Tree ID	Description	Scenario(s)	$I_{RWS}$
F.L.	Filter leak	All	1.720
TPRD.P	TPRD prematurely opens	All	1.399
TPRD.L	TPRD leak	All	1.328
CHV.FTC	Check valve failure to close	All	1.025
CHV.L	Check valve leak	All	1.007

Medium Pressure			
Fault Tree ID	Description	Scenario(s)	$I_{RWS}$
PRD1.FR	PRD1 failure to recast	All	1.874
PRD1.L	PRD1 leak	All	1.552
PRD1.P	PRD1 prematurely opens	All	1.212
Reg2.L	Regulator 2 leak	All	1.0013
Reg2.FTO	Regulator 2 failure to open	All	1.0009

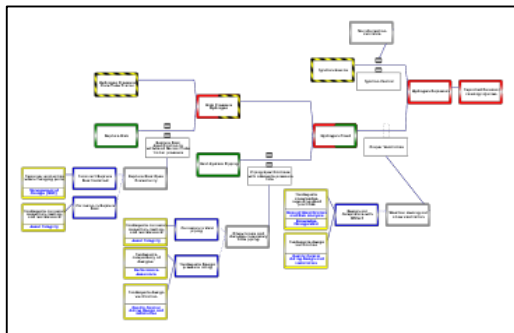
- Shows extended types of impactful outputs possible from using QRA:
- Calculated worker risk (FAR) and compared to U.S Gov't (BLS) data for industrial truck & material handling occupation fatalities.
- Identified most risk-significant components using importance measures analysis – potential to inform design modifications and/or codes and standards.

Copyright, Katrina Groth, 2025

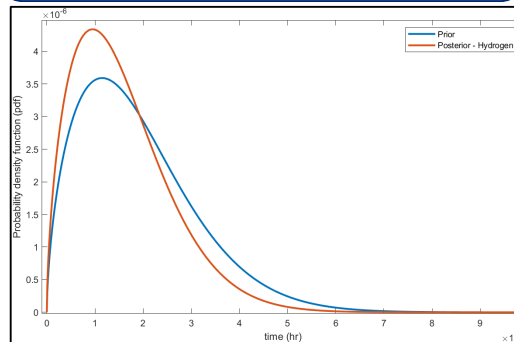
# Evaluating the risk trade-offs of pressure relief devices in hydrogen systems

**Objective:** Define a probabilistic failure model for pressure relief devices (PRD) installed in hydrogen services to assess the risk trade-off they provide.

Establish risk management needs by identifying PRD incidents



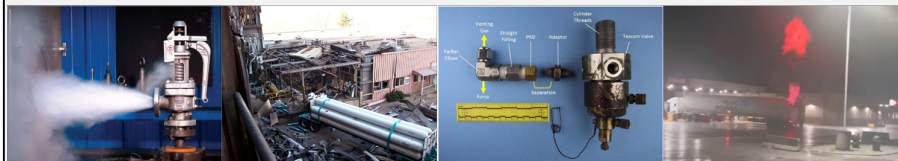
Define probabilistic failure models for PRDs installs on hydrogen systems



Assess the risk provided by PRDs in fueling station and evaluate trade-offs



- Previous studies have shown that PRDs do not receive the attention they need in regard to risk.
- Hydrogen introduces new challenges, and there are no models to evaluate the risk of PRDs



## **Implications & Impact:**

- First of its kind in analyzing PRD risk profile, allowing the balance between risk control vs risk provided
- Inform industry and stakeholders about **risks and mitigation options** for PRDs
- Inform Code & Standards Committees on when to use PRDs as risk control mechanism.



Pressure Relief Valves



Burst or Rupture Disc

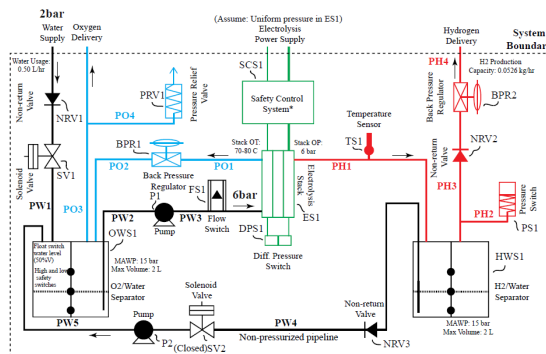
A. Jimenez and K. M. Groth, "Hazards Associated with Pressure Relief Devices in Hydrogen Systems," *Journal of Loss Prevention in the Process Industries*, vol. 91, p. 105380, Oct. 2024.

# Early insights from QRA on H2 electrolyzers

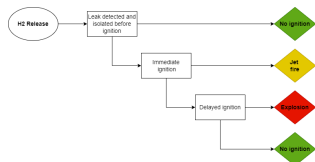


**Objective:** Conduct QRA for an electrolyzer system to inform hydrogen technology development and QRA development to support hydrogen risk mitigation measures. In addition, the project seeks to identify input data gaps for hydrogen system QRA and any additional R&D needs in this topical area.

## Lab-scale PEM electrolysis system



## Event sequences



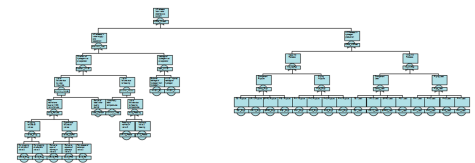
- For an H<sub>2</sub> release, jet fires are twice as likely to occur vs. explosions.
- The most risk-significant events for H<sub>2</sub> releases are:
  - External and internal leakage of hydrogen in hydrogen-water separator
  - Flow restrictions of the non-return and solenoid valves connecting the two gas-water separators
  - External leakage of hydrogen from non-return valve, backpressure regulator, and piping in H<sub>2</sub> production

## FMEA

Component ID	Component Name	Failure Mode	Effect of Failure Mode	Consequence of Failure Mode	Severity	Frequency	Rank
1	Water Supply	Water supply failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	1
2	Oxygen Supply	Oxygen supply failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	2
3	Back Pressure Regulator	Back pressure regulator failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	3
4	Flow Switch	Flow switch failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	4
5	PEM Electrolyzer	PEM electrolyzer failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	5
6	Solenoid Valve	Solenoid valve failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	6
7	Pressure Regulator	Pressure regulator failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	7
8	Hydrogen Separator	Hydrogen separator failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	8
9	Water Separator	Water separator failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	9
10	Piping	Piping failure	Electrolyzer shutdown	Loss of hydrogen production	High	Low	10

- Water supply and separation is the highest contributor to # of high-risk scenarios leading to an H<sub>2</sub> release.
- Electrolysis and O<sub>2</sub> production contribute to nearly 60% of # of high-risk scenarios leading to H<sub>2</sub>-O<sub>2</sub> mixing.

## FT analysis

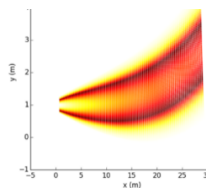


- In terms of frequency, H<sub>2</sub>-O<sub>2</sub> mixing is the most frequently-occurring top event in electrolyzer operations (between a H<sub>2</sub> release, O<sub>2</sub> release, and H<sub>2</sub>-O<sub>2</sub> mixing)

## Importance measures analysis

Fault Tree ID	Description	IRRW
HWS1_EL	External leak of hydrogen from hydrogen-water separator	3.62
HWS1_IL	Internal leak of hydrogen from hydrogen-water separator	1.36
SV2_Plug	Solenoid valve 2 plugged	1.00
SV2_FTO	Solenoid valve 2 fails to open	1.00
SV2_FC	Solenoid valve 2 fails closed	1.00

## Release & flame simulations



$$Pr_{thermal\ harm} = 2.56 \times 10^{-22}$$

$$Pr_{overpressure\ harm} = 0.95$$

## Scenario Analysis & Total risk (FAR, AIR)

	AIR (fatalities/electrolyzer-year-operator)	FAR (fatalities/100E+6 hours-operator)	Expected fatalities/year
Major H2 release leading to a jet fire	$1.14 \times 10^{-26}$	$2.82 \times 10^{-22}$	$6.25 \times 10^{-25}$
Major H2 release leading to an explosion	$2.03 \times 10^{-5}$	$5.09 \times 10^{-1}$	$1.12 \times 10^{-3}$
Total	$2.03 \times 10^{-5}$	$5.09 \times 10^{-1}$	$1.12 \times 10^{-3}$

## Early QRA results for electrolyzers show the importance of:

- Mechanical integrity and leak detection for electrolyzer stack, gas-water separators and valves
- Preventing freezing, plugging (flow blockage) in valves in H<sub>2</sub>-Water separation
- Increased interior volume and/or venting of H<sub>2</sub> from the enclosure of the system

# Quantitative Risk Assessment of the Safety and Reliability of Proton Exchange Membrane Electrolysis for Hydrogen Production at Nuclear Power Plants



## Objective:

Establish technical foundations and processes for assessing the safety of hydrogen production in nuclear power plant (NPP) applications by conducting and documenting a comprehensive QRA on a proton exchange membrane (PEM) electrolysis facility coupled to a NPP.

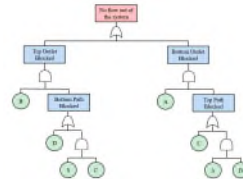
### Task 1:

Conduct a **failure modes and effects analysis** on the PEM electrolyzer

Probability Class	High	M	H	H
	Medium	L	M	H
	Low	L	L	M
		Minor	Moderate	Critical
		Severity Class		

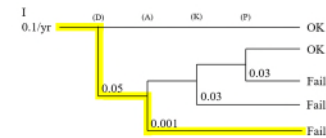
### Task 2:

Develop **fault trees** by functional group for risk critical scenarios



### Task 3:

Create **event sequence diagrams** to model undesired consequences



### Task 4:

Simulate and incorporate **consequence simulations** into ESDs

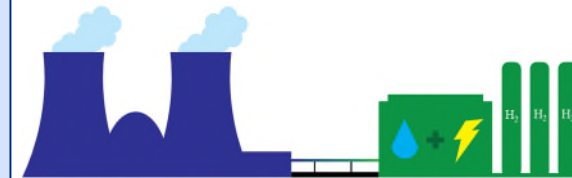


## Expected Results:

- **Fully documented QRA** for the safety and reliability of the PEM electrolyzer coupled to the NPP
- **Identification of the most risk significant components** from the PEM electrolyzer design
- Risk informed PEM electrolyzer **design and layout recommendations**

## Impact:

- Ensure that siting the nuclear and hydrogen facilities together does not impose undue risk **through making early stage design and layout recommendations**
- Enable a **transition to decarbonized nuclear hydrogen production**, at scale, to support transportation, industrial manufacturing, and energy storage

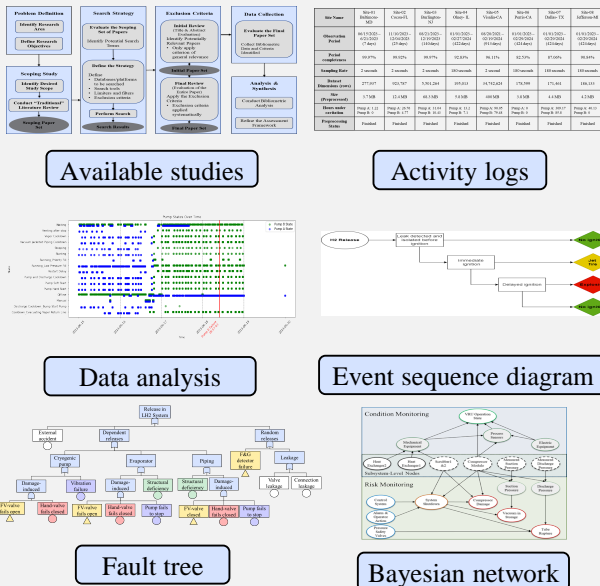




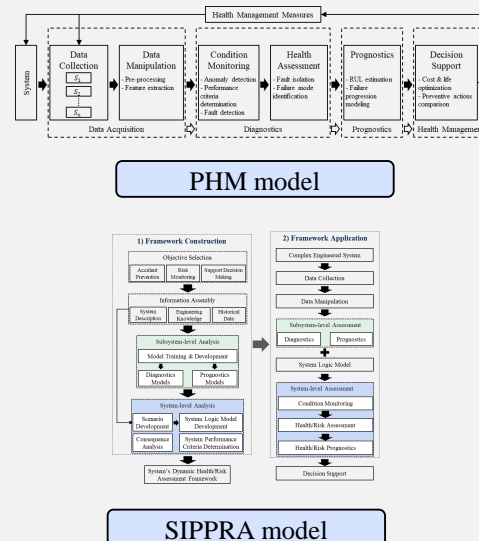
# Cryogenic pump reliability project: Objective & Motivation

- Objective:** Develop mechanistic & computational understanding of the failure modes, behaviors, and mechanisms for cryogenic pumps and develop reliability models and methods to predict when these events will occur.

## Data gathering and evaluation



## Model development and reliability analysis



## Advanced monitoring and maintenance practices

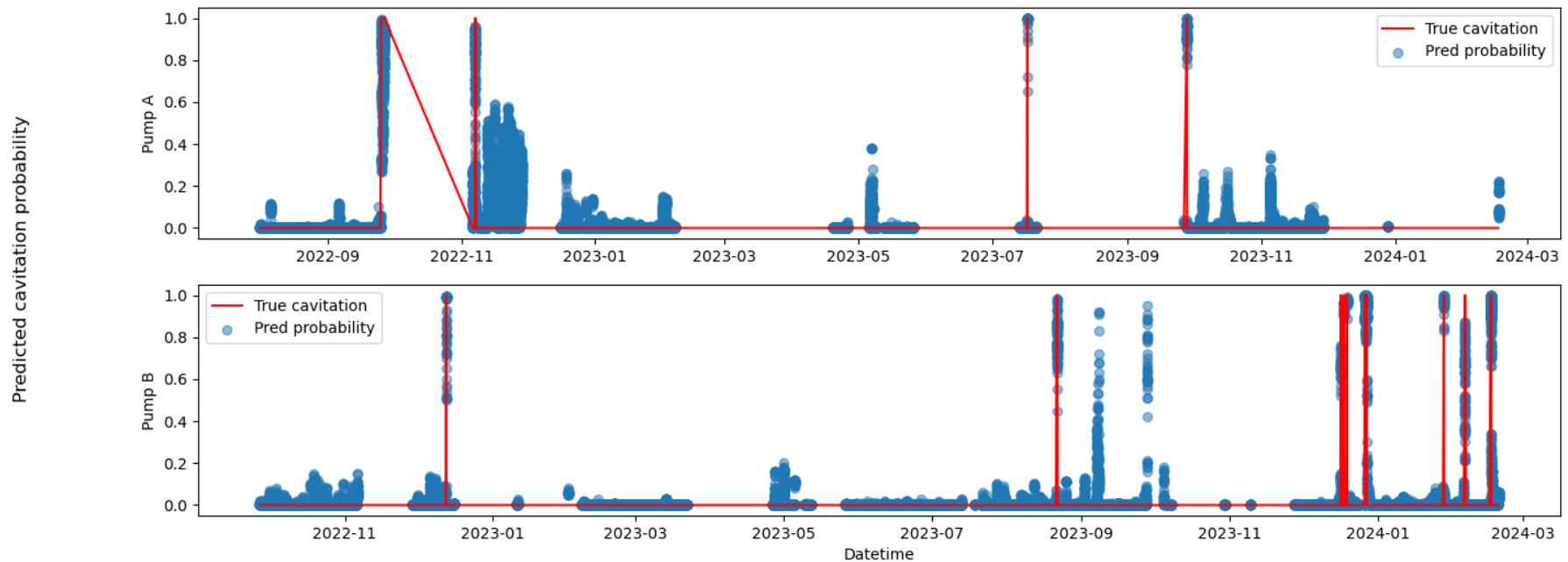


Plug hydrogen storage and handling facility

# Cavitation data-driven machine learning model



Developed data-driven model for predicting cavitation from 3+ years of data with a handful of cavitation events

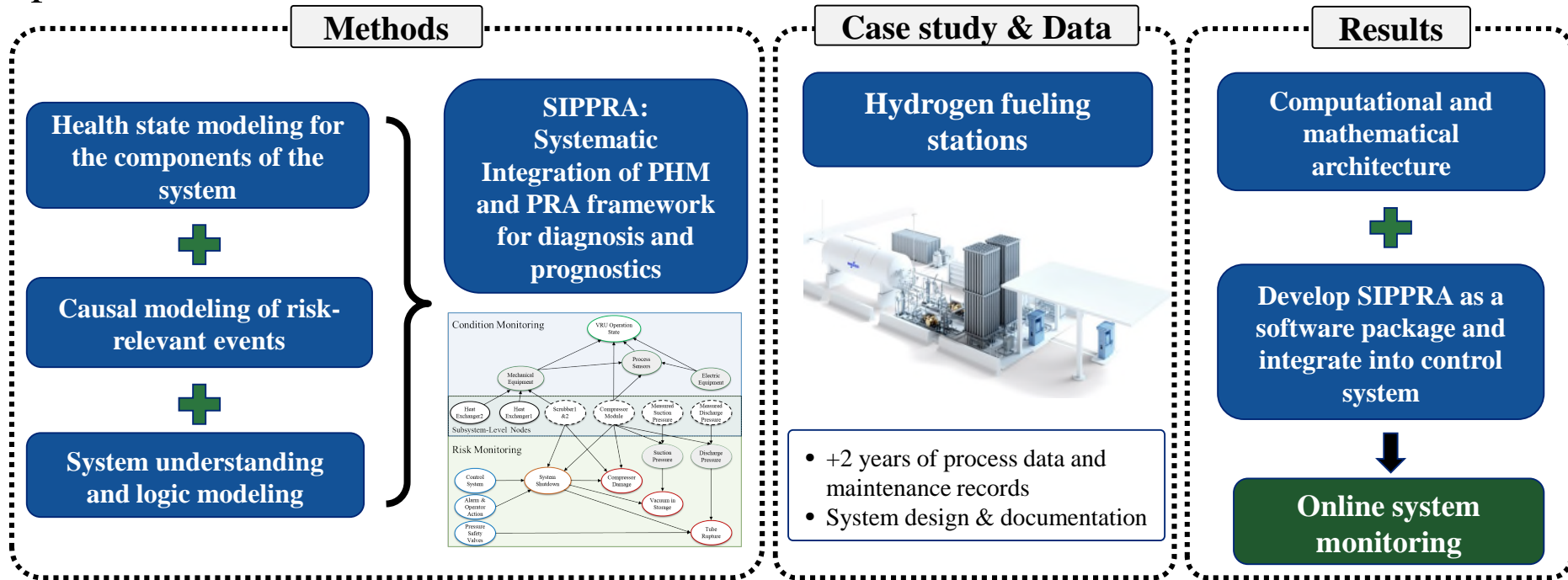


- Model is uncovering cavitation events that were undetected
- Cavitation events can be detected minutes earlier than previous algorithm
- This analysis uncovered a timing mismatch in maintenance records -- customer is correcting the record reporting.

# A methodology for Risk and Reliability Prognostics applied to Hydrogen Fueling Stations

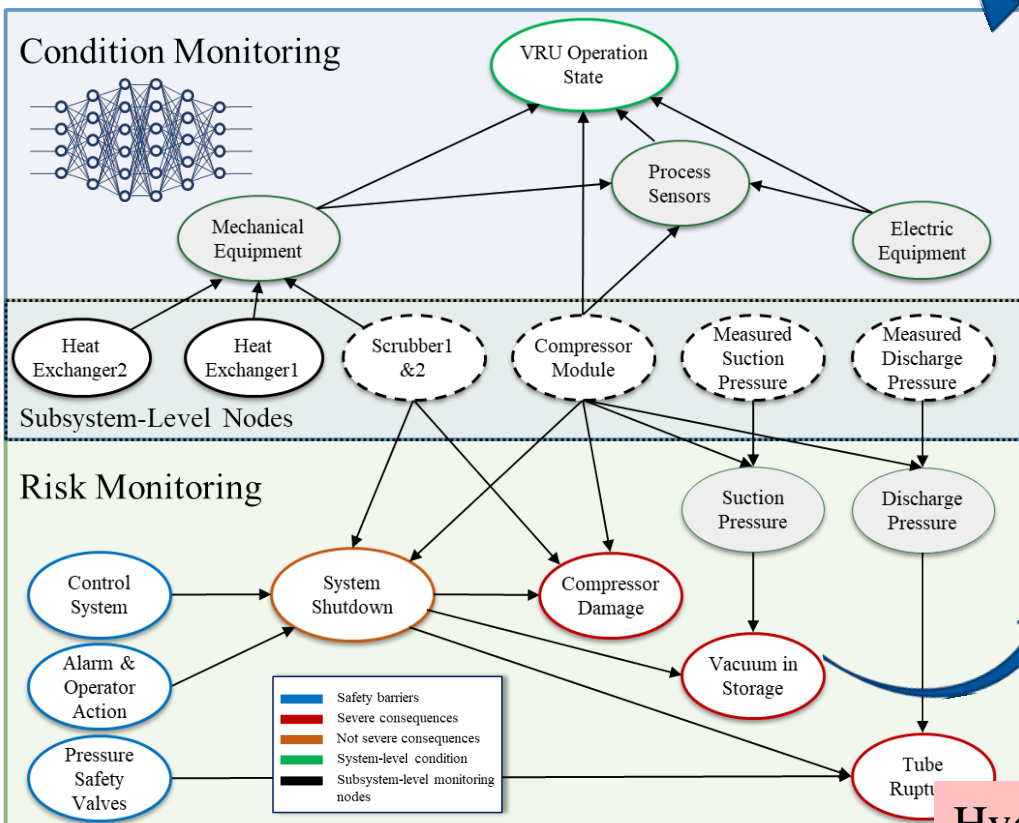


**Research objective:** Create a framework for system-level health state and risk prognostics on energy systems by fusing system understanding, causal logic and process data



This methodology will monitor system risk and estimate remaining useful life (RUL) of critical components, enabling more reliable operation and efficient maintenance planning

# SIPPRA Example: day-to-day operations – risk monitoring of an oil & gas vapor recovery unit



Hydrogen system case study coming soon

Our new methods can dynamically monitor the risk of complex engineering systems

Copyright, Katrina Groth, 2025

# Research defining a Hydrogen Component Reliability Database (HyCReD)



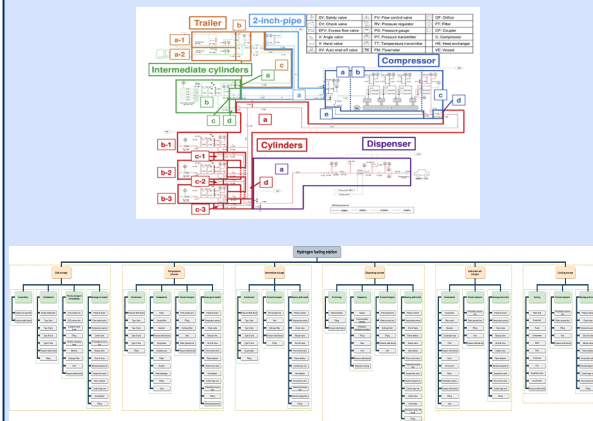
## Evaluated existing H2 safety data collection tools

	Data Type	H2Tools	NREL CDPs	HIAD	CHS Failure Rate Data
Event and failure characterization	Initiating event (description)	✓	✓	✓	✓
	Location within system	×	×	0	×
	Failure mode	×	×	×	×
	Failure mechanism	×	×	×	×
	Failure root cause	✓	✓	✓	×
	Release size	×	0	✓	✓
	Incident severity	✓	✓	✓	✓
	Consequences	0	✓	✓	0
	System response (Mitigation)	×	×	×	0
	H2 accumulation	×	×	×	×
Life/usage	H2 detection	×	×	×	0
	Component life	×	×	×	×
	Operations	×	✓	×	0
	Maintenance	×	✓	×	0
	Site inventory	×	✓	×	0
Data scope	Public access to data	✓	×	✓	?
	Scope includes any H2 incident	✓	×	✓	✓
	Regular reporting	×	✓	×	✓
	Anonymous data presentation	✓	✓	✓	✓
	Data quality checks	×	×	×	?
	Process documentation	×	×	0	×

## Defined requirements for HyCReD

Characteristics	Static data	Failure event data	Maintenance event data
<ul style="list-style-type: none"> <li>Design for usability</li> <li>Publicly available</li> <li>Regular reporting</li> <li>Anonymity</li> <li>Quality assurance</li> <li>Regular updating</li> <li>Process documentation</li> </ul>	<ul style="list-style-type: none"> <li>Component location</li> <li>Operating condition</li> <li>Component life</li> <li>Number of like components</li> </ul>	<ul style="list-style-type: none"> <li>Narrative event description</li> <li>Failure mode</li> <li>Failure mechanism</li> <li>Root cause</li> <li>Release location &amp; size</li> <li>Hydrogen accumulation</li> <li>Detection</li> <li>Isolation</li> <li>Consequence</li> <li>Severity</li> </ul>	<ul style="list-style-type: none"> <li>Type of maintenance</li> <li>Maintenance action performed</li> <li>Active repair time</li> <li>Manhours</li> </ul>

## Developed system-specific H2 fueling station decomposition



## Defined hydrogen-specific component failure modes

Failure Mode	Definition
Abnormal output-high	Above normal output indicates potential failure(s)
Abnormal output-low	Below normal output indicates potential failure(s)
Bent/warped/damaged	Visible damage
Contamination	Component allows foreign material to contaminate product
Drift	Erroneous reading due to lack of calibration
Erratic output	Inconsistent output
External leak hydrogen	Hydrogen leak from within system to environment
External leak utility medium	Utility medium leak from the system to the environment
External rupture hydrogen	Complete loss of containment. Hydrogen expands to the environment
External rupture utility medium	Complete loss of utility medium to the environment
Fail closed	Component stops working in the closed position
Fail open	Component stops working in the open position
Fail to close	Component does not close on demand
Fail to disconnect	Component's intent to disconnect does not do so on demand
Fail to expurge	Hydrogen remains in liquid form after passing through expurgator
Fail to operate	Component does not function on demand
Fail to stop	Component does not stop on demand
Freezing	Component is frozen and becomes inoperable/requires maintenance
Insufficient heat transfer	Target parameters for temperature are not met in a heat exchanger
Internal leak hydrogen	Hydrogen leak within system boundary (e.g. across a closed valve)
Internal leak utility medium	Utility medium leak within system boundary (e.g. across a closed valve)
Internal rupture hydrogen	Complete loss of containment. Hydrogen stays within the system boundary
Internal rupture utility medium	Complete loss of containment. Utility medium stays within the system boundary
Open circuit	Electrical circuit that is not complete
Overheating	Component is exposed to temperatures above design specifications
Over-speed	Component operates above desired/specified speed
Plugging	Buildup of material restricting flow
Restricted flow	Component is restricting flow when not intended to do so
Short circuit	Division of current
Spurious operation	Activation without specified demand (components normally idle)
Spurious stop	Stop without specified demand (components normally active)
Stuck connection	Component is stuck at point of contact (nozzle)
Under-speed	Component operates below desired/specified speed

## Developed & validated HyCReD structure

### Static data fields

Event Number	Station/Facility Identification	Facility Type	Service/Usage	Nominal Working Pressure	H2 phases on site
25	A	Commercial, public	Heavy-duty	700 bar	Gas
26	B	Research, limited-access	Both heavy- and light-duty	350 bar	Gas

Event Number	Equipment Description	Subsystem	Functional Group	Component	Component Nominal Working Pressure	Component Population	P&ID Part Number
25		Bulk storage	Containment	Type III tank	250-300 bar	18	TK-103
26		Compression process	Compression	Compressor	400-680 bar	2	CO-E-49A

### Failure event data fields

Event Number	Time & Date of Failure	Failure Mode	Failure Severity	Failure Mechanism	Failure Root Cause Description	Hydrogen Release (Yes/No)	Release Size (Small/Medium/Large)	Ignition (Yes/No)
25	07/17/2021 08:32	External leakage-Process medium	Critical	Leakage		Yes	Medium	No
26	10/17/2021 15:33	Parameter deviation	Degraded	Overheating		No	Small	No

### Maintenance event data fields

Date & Time Repair Started	Date & Time Repair Completed	Date & Time Station Restarted	Action Performed	Maintenance Description
07/18/2021 09:55	07/28/2021 10:00	07/29/2021 09:30	Replacement	
10/17/2021 17:30	10/20/2021 13:30	10/20/2021 15:30	Repair	

Copyright, Katrina Groth, 2025

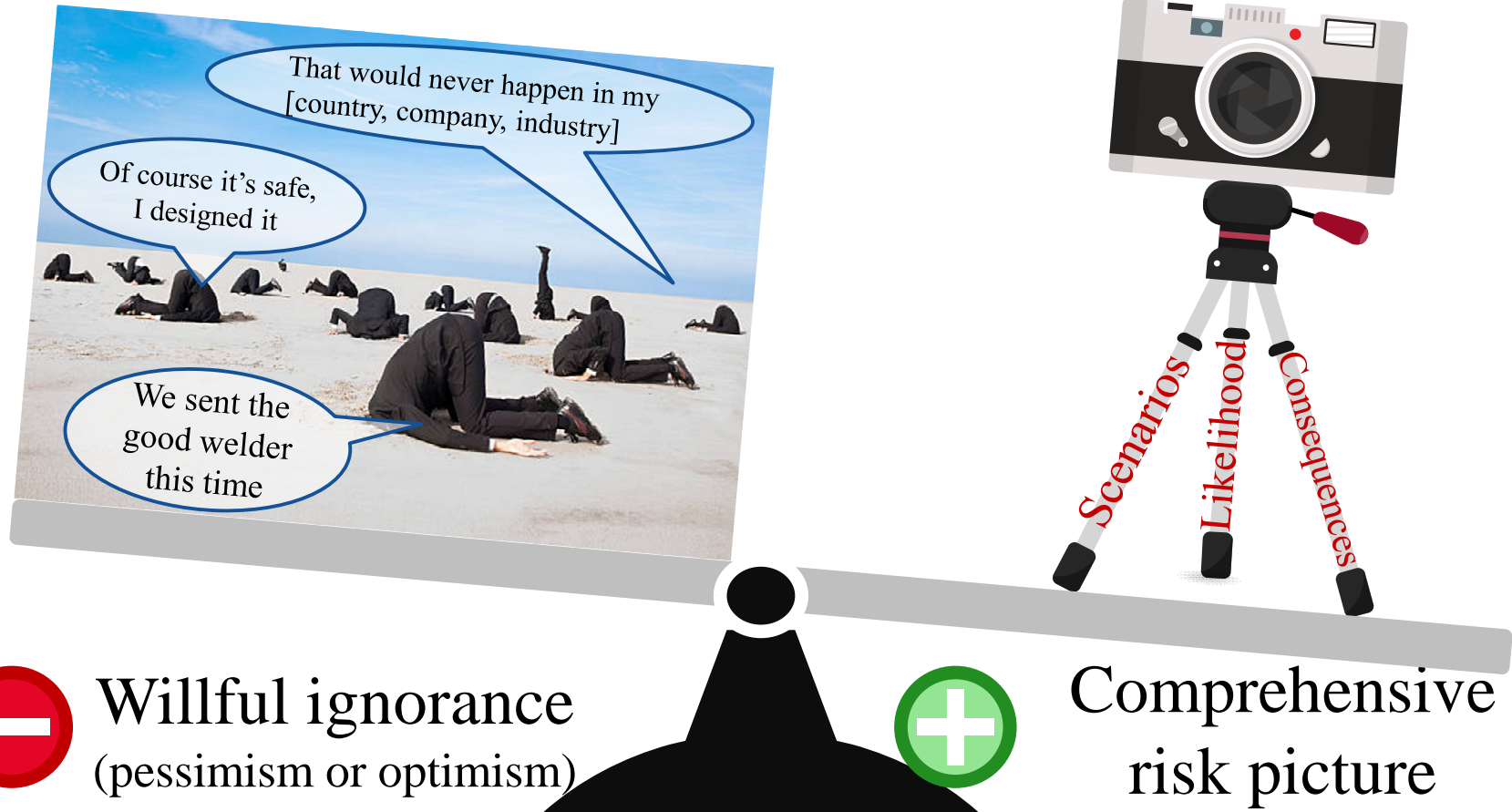




*“Failures are the accidental experiments that contribute to the engineer’s experience.... Finding the true causes of failure often takes as much of a leap of the analytical imagination as original design concepts.”*

*-- Henry Petroski, To Engineer Is Human: The Role of Failure in Successful Design, 1992.*

# Principles: Why QRA?



# Key takeaways & Closing thoughts

- Systems must be engineered for safety & reliability
- QRA & Process Safety *enable* hydrogen system safety
  - Need to scale-up QRA analysis as the industry matures to enable mitigation of early design/deployment issues
  - Opportunities to partner – what can we do together to advance the state of knowledge?

Advances in risk analysis & reliability engineering for hydrogen systems will continue to drive the industry forward

# Acknowledgements – SyRRA Lab Members & Sponsors



Research supported by multiple sources. The views expressed herein are those of the authors and do not reflect the official policy or position of any sponsor.



Center for Risk and  
Reliability

University of Maryland  
Reliability Engineering  
Center for Risk and Reliability

Center for Risk and Reliability:  
<http://crr.umd.edu>

The views expressed in this presentation are those of the author and do not reflect the official policy or position of the sponsors.

# Center for Risk and Reliability



A. JAMES CLARK  
SCHOOL OF ENGINEERING